

# Biological removal of siloxanes from biogas for biomethane injection in natural gas grid

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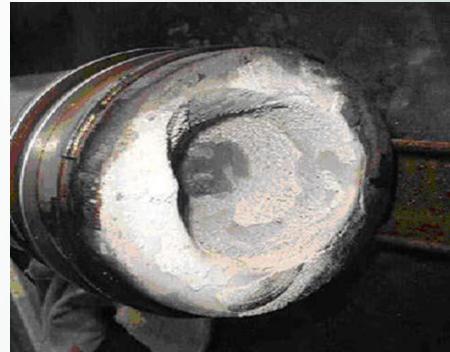
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# INTRODUCTION

- Biogas contains trace level concentrations of volatile methyl siloxanes (VMS)



- Decreased efficiency of the equipment
  - Corrosion
  - Erosion
  - Clogging of pipes
- Increased maintenance costs



- Removal of VMS from biogas prior energy valorization is mandatory

Siloxanes concentration in biogas = 20-400 mg m<sup>-3</sup>



Maximum concentration for biomethane injection in natural gas grid

10 mg m<sup>-3</sup>



# INTRODUCTION

## ➤ Conventional physical-chemical processes for siloxanes removal:

- High operating and investment cost

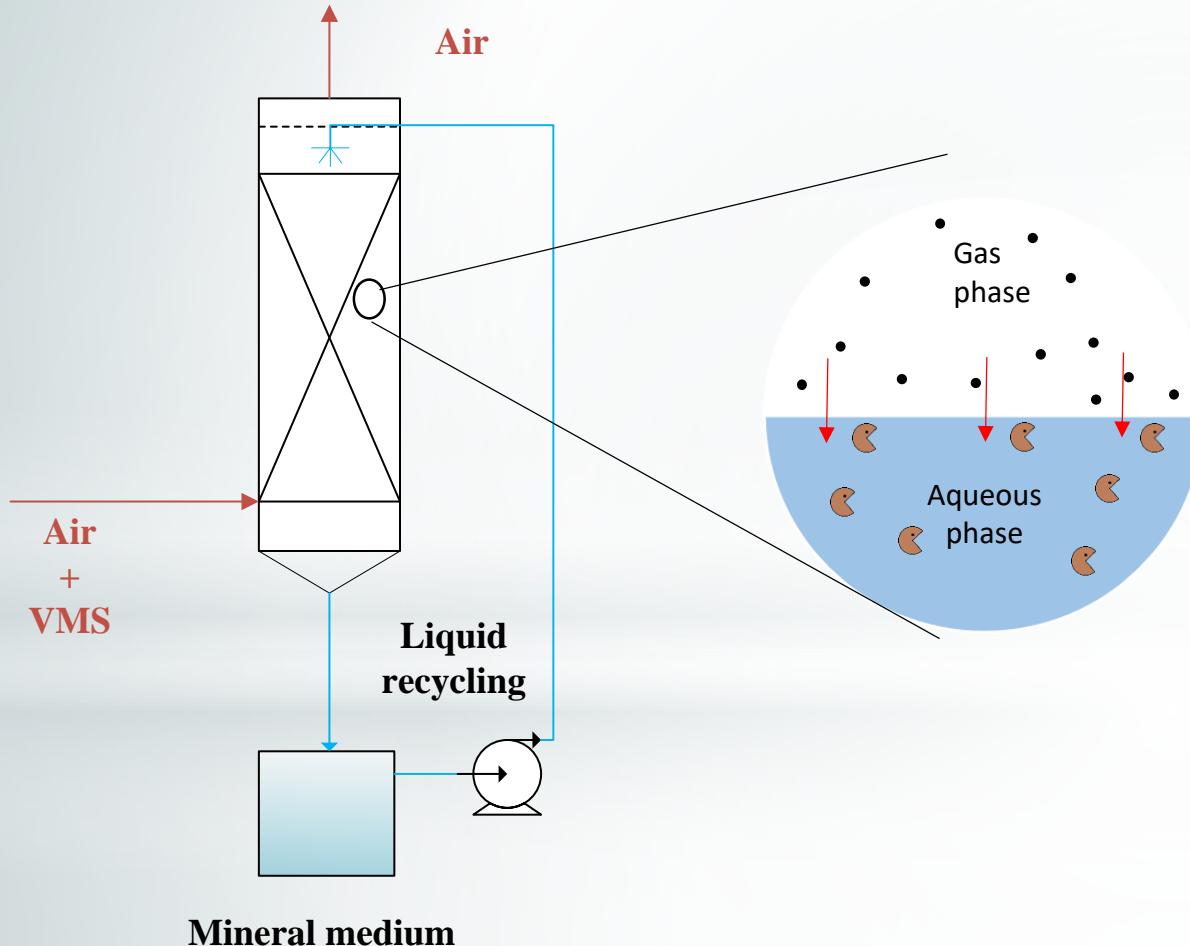
Physical-chemical processes	RE (%)	Disadvantages
Adsorption	90-99	Regeneration/replacement of the adsorbent
Absorption	> 90	Cooling to avoid organic solvent emissions Corrosive nature of acid solutions Alkaline deposits (alkaline absorbent solutions)
Cryogenic condensation	> 90	Extreme operating temperatures (-25, -70 °C)
Membrane separation	> 80	Compressors or vacuum pumps energy consumption

## ➤ Biological processes:

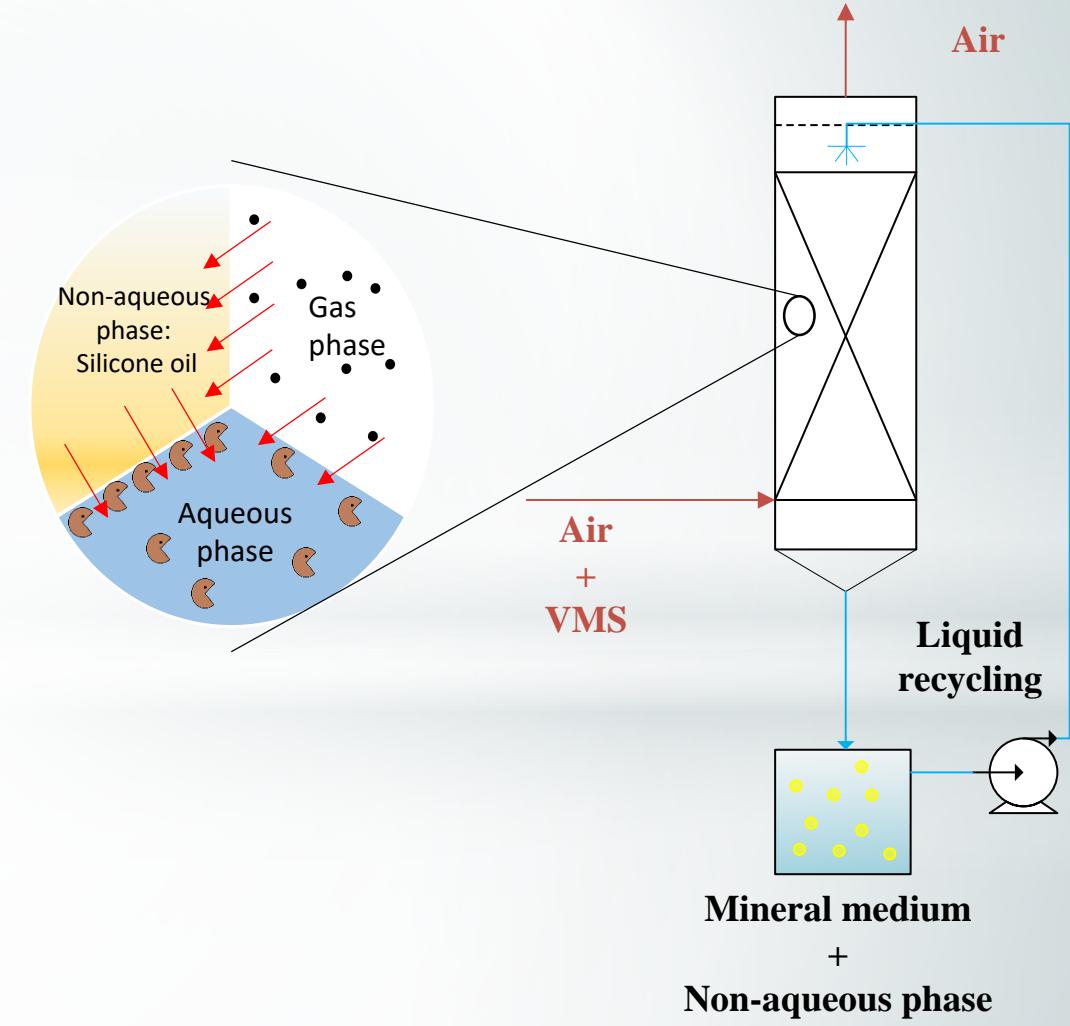
- Low-cost
- Environmentally friendly



# Biotrickling Filters (BTFs)

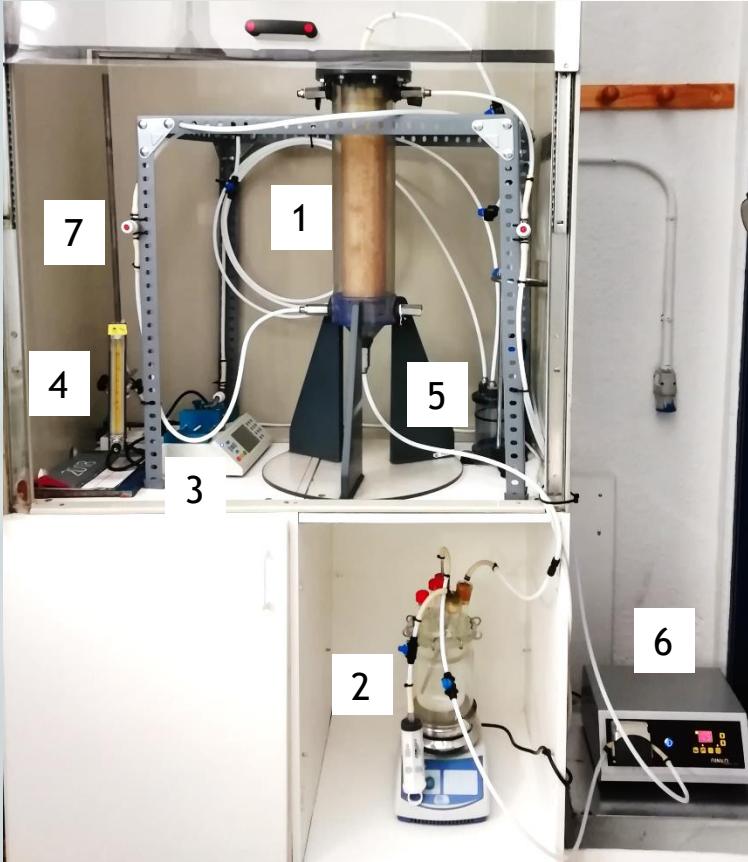


One-phase biotrickling filter (1P-BTF)

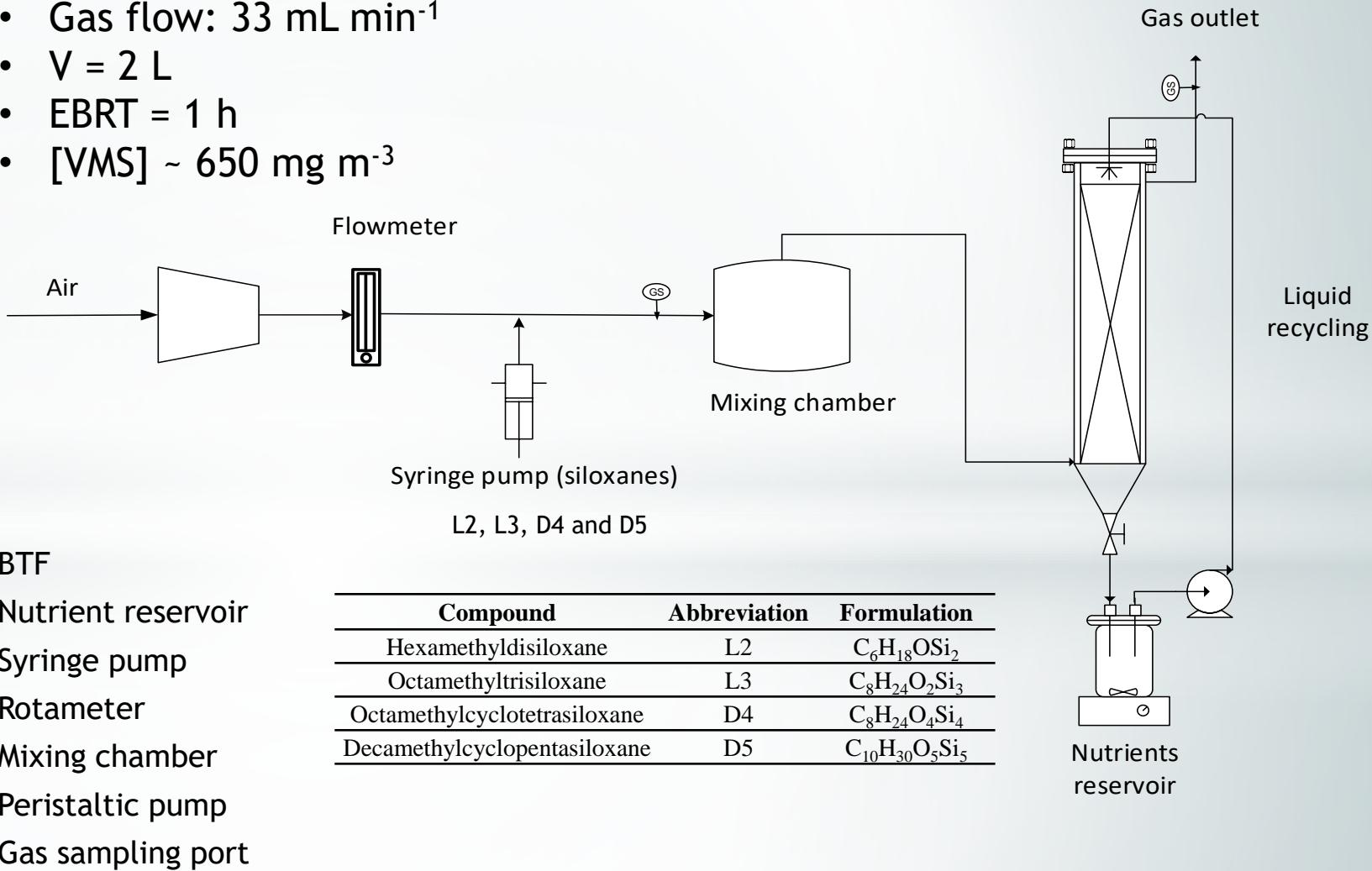


Two-phase partitioning biotrickling filter (TP-BTF)

# BTFs: Experimental setup

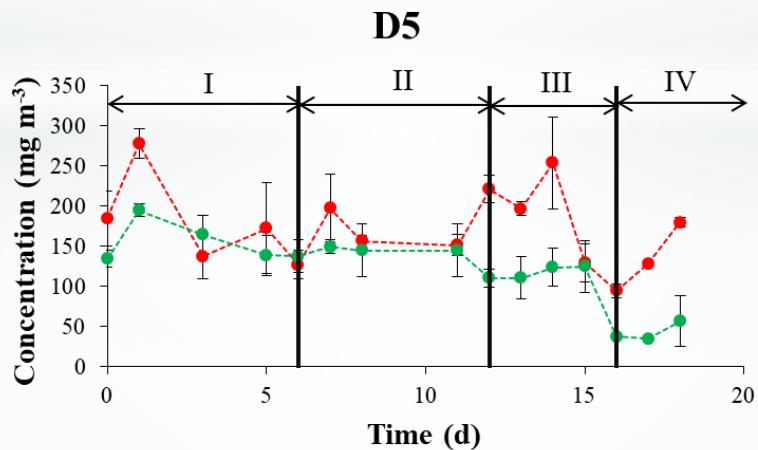
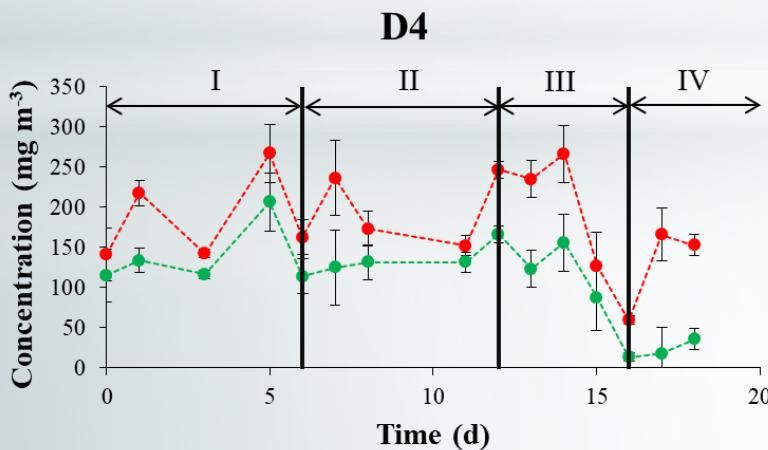
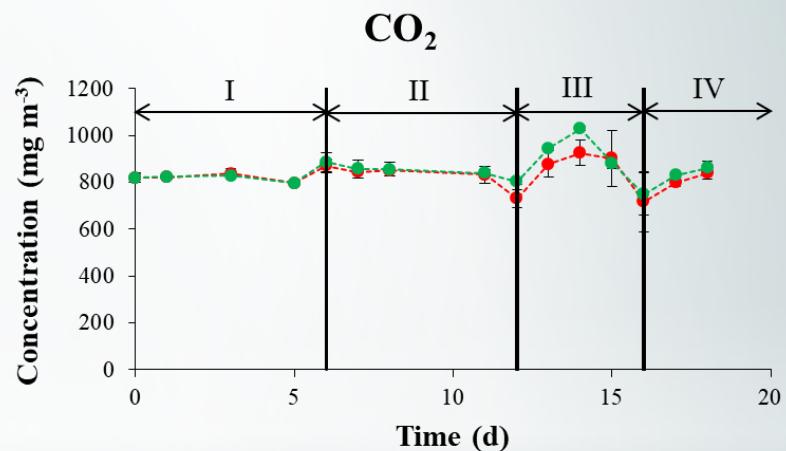
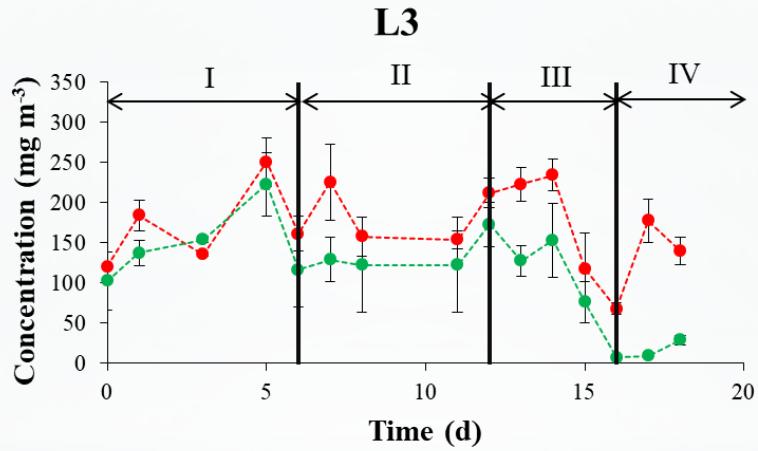
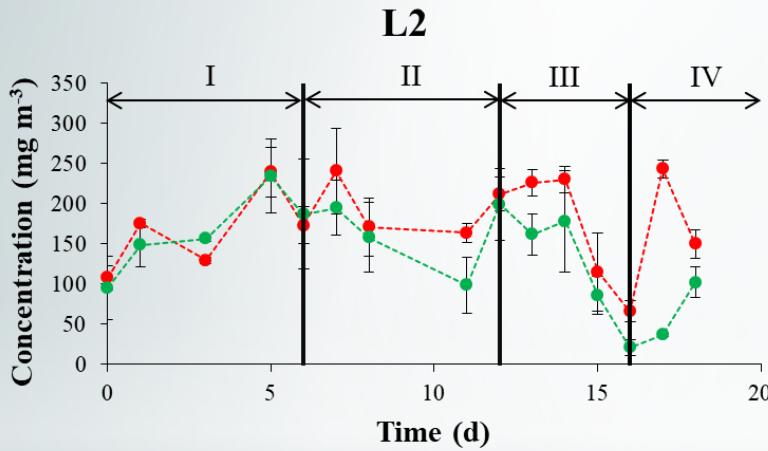


- Gas flow:  $33 \text{ mL min}^{-1}$
- $V = 2 \text{ L}$
- EBRT = 1 h
- $[\text{VMS}] \sim 650 \text{ mg m}^{-3}$



- 1- BTF
- 2- Nutrient reservoir
- 3- Syringe pump
- 4- Rotameter
- 5- Mixing chamber
- 6- Peristaltic pump
- 7- Gas sampling port

# BTFs: Abiotic test



Inlet concentration (●)  
Outlet concentration (○)  
PVC column (I)  
Packing material (II)  
Mineral medium (III)  
Mineral medium + silicone oil (IV)

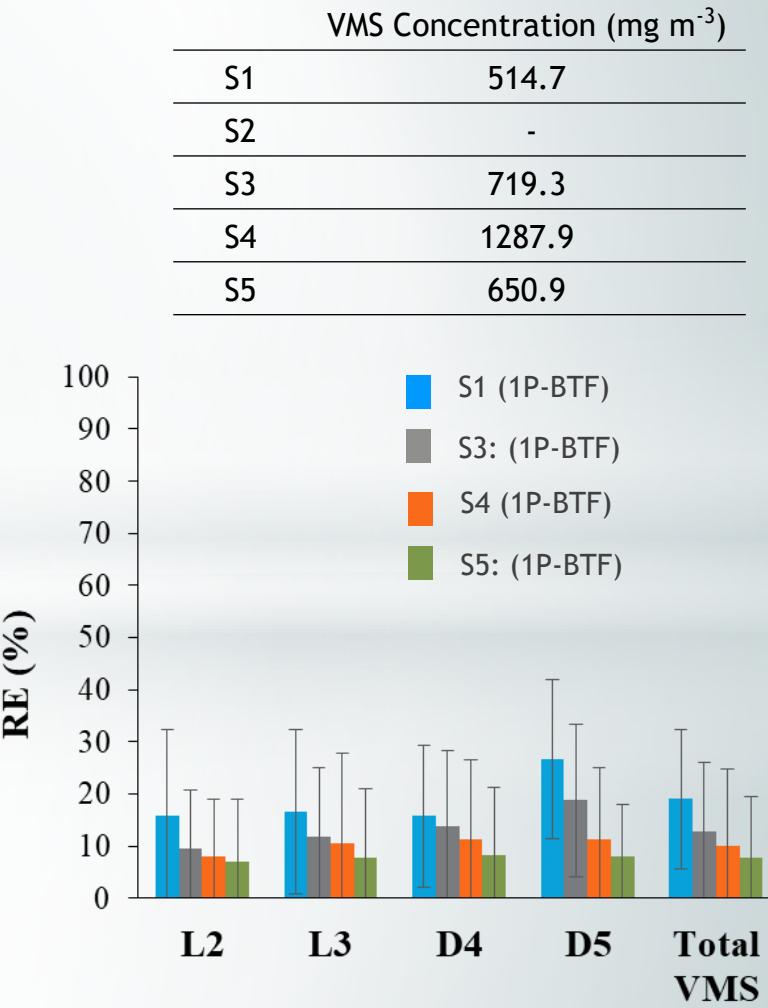
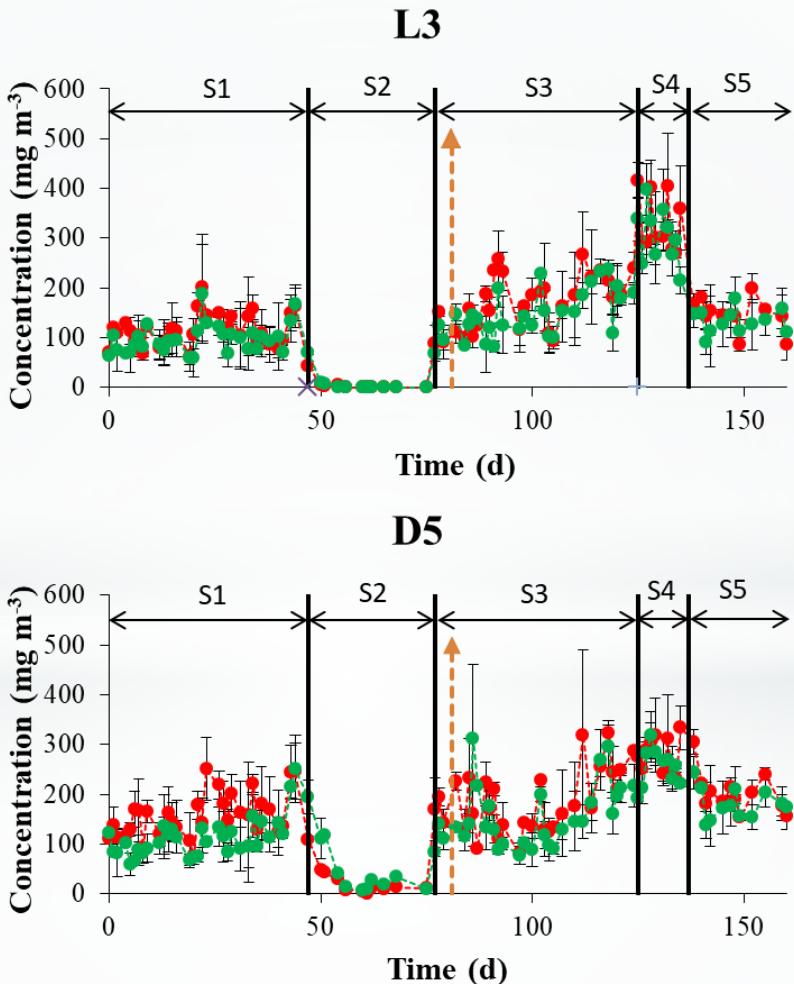
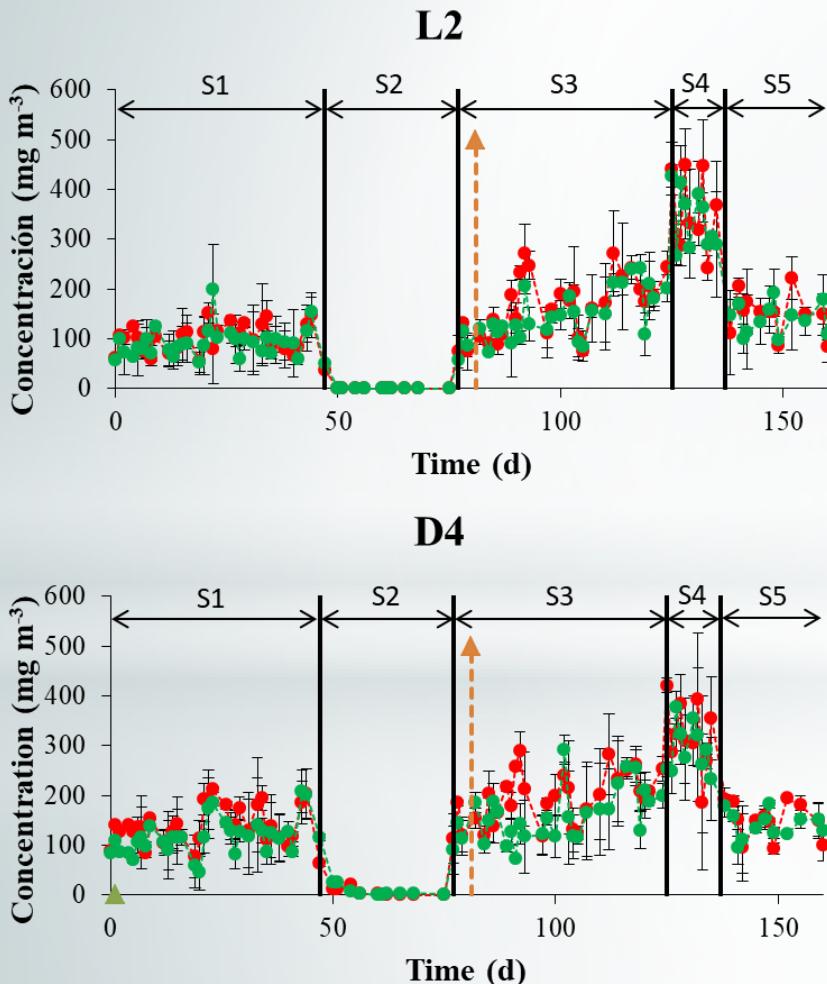
# BTFs: Experimental conditions

1P-BTF	Feed Stream	Time curse (Days)	VMS Concentration ( $\text{mg m}^{-3}$ )
S1	VMS loaded air stream	0 - 46	$514.7 \pm 125.6$
S2	Clean air stream	47 - 76	-
S3	VMS loaded air stream	77 - 124	$719.3 \pm 203.4$
S4	VMS loaded air stream	125 - 137	$1287.9 \pm 216.8$
S5	VMS loaded air stream	138 - 160	$650.9 \pm 126.9$

TP-BTF	Feed Stream	Time curse (Days)	VMS Concentration ( $\text{mg m}^{-3}$ )
S1	VMS loaded air stream	0 - 21	$624.0 \pm 172.4$
S2	Clean air stream	22 - 70	-
S3	VMS loaded air stream	70 - 113	$640.0 \pm 198.0$



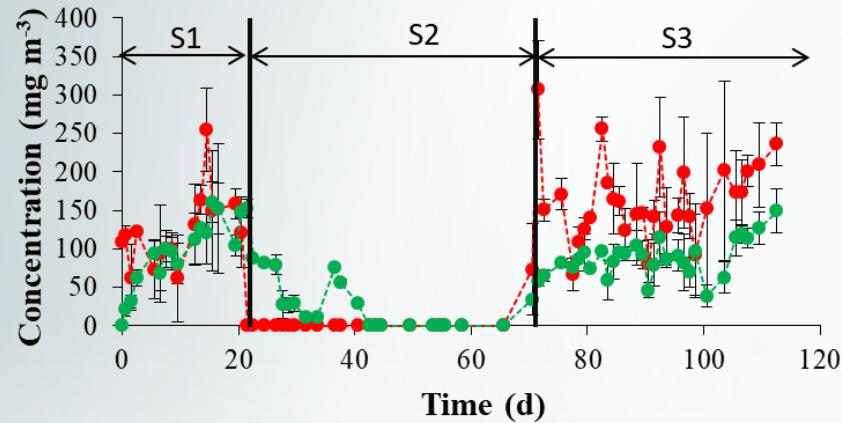
# 1P-BTF: VMS concentration and RE



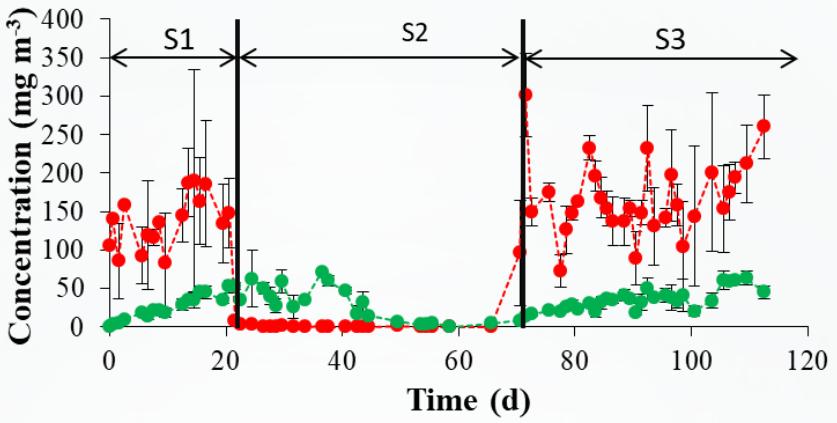
Inlet concentration (●)  
Outlet concentration (●)  
Day 81: System reinoculation (→)

# TP-BTF: VMS concentration and RE

**L2**



**L3**



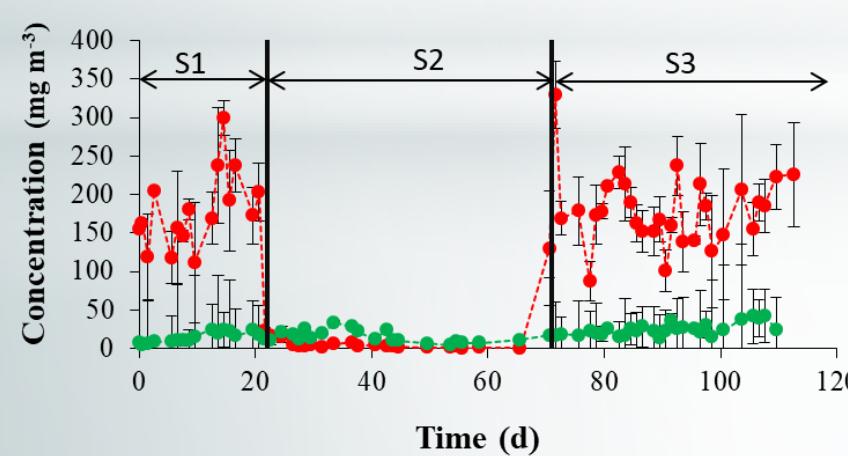
VMS Concentration ( $\text{mg m}^{-3}$ )

S1	624.0
S2	-
S3	640.0

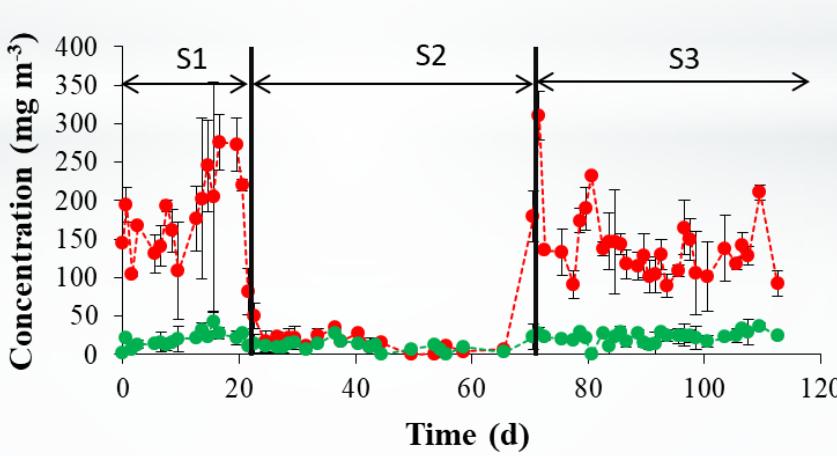
S1 (TP-BTF)

S3: (TP-BTF)

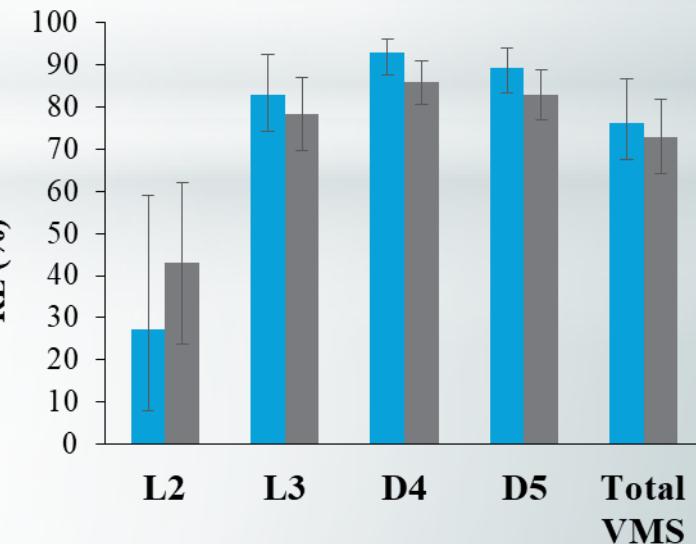
**D4**



**D5**

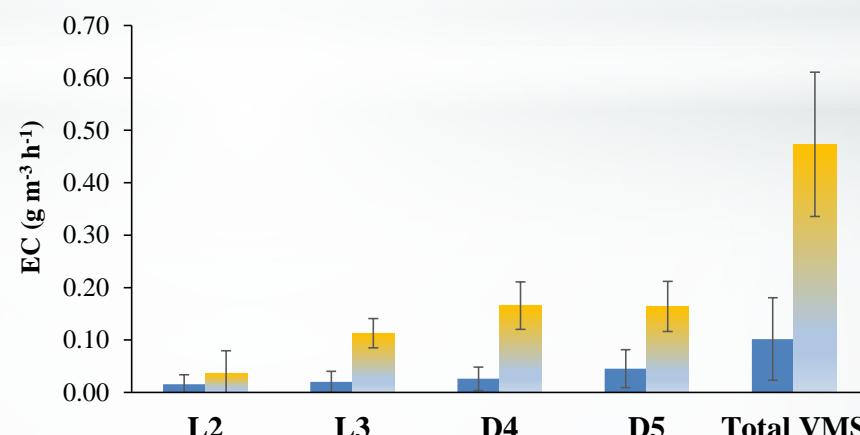
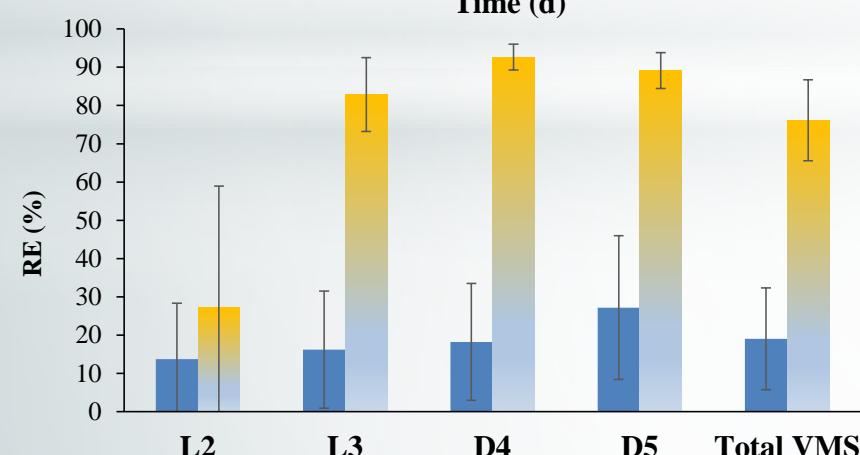
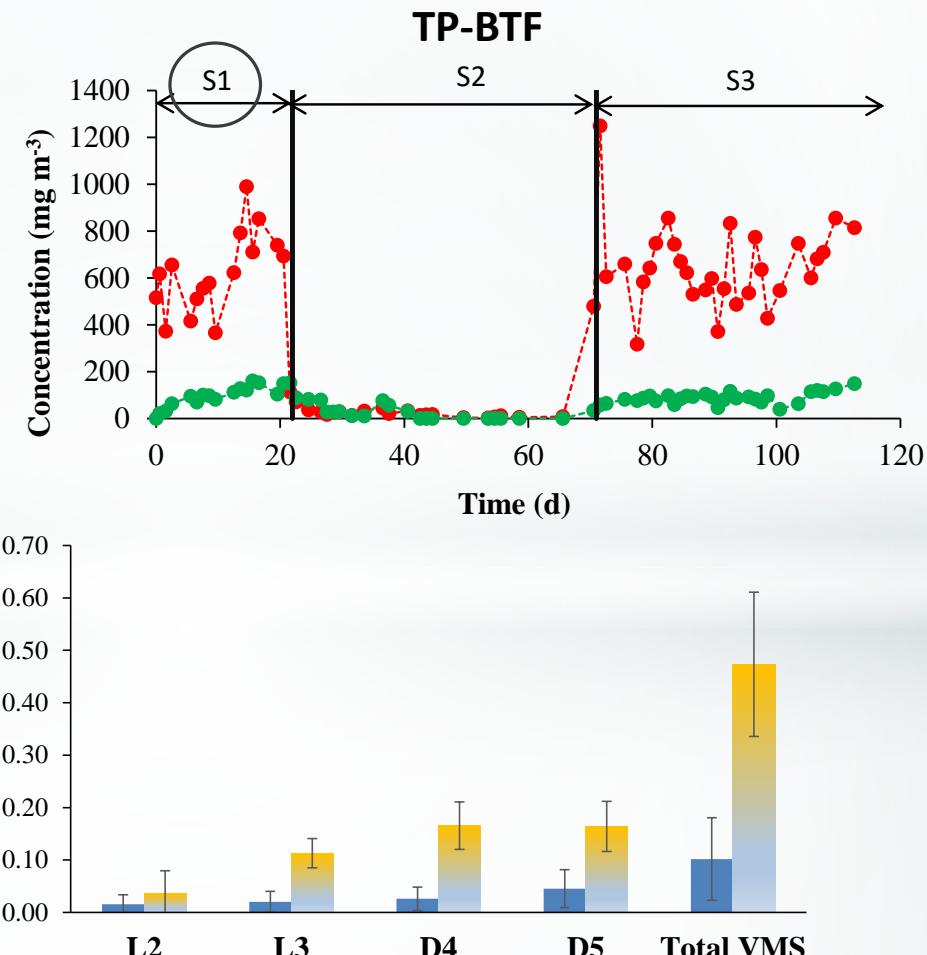
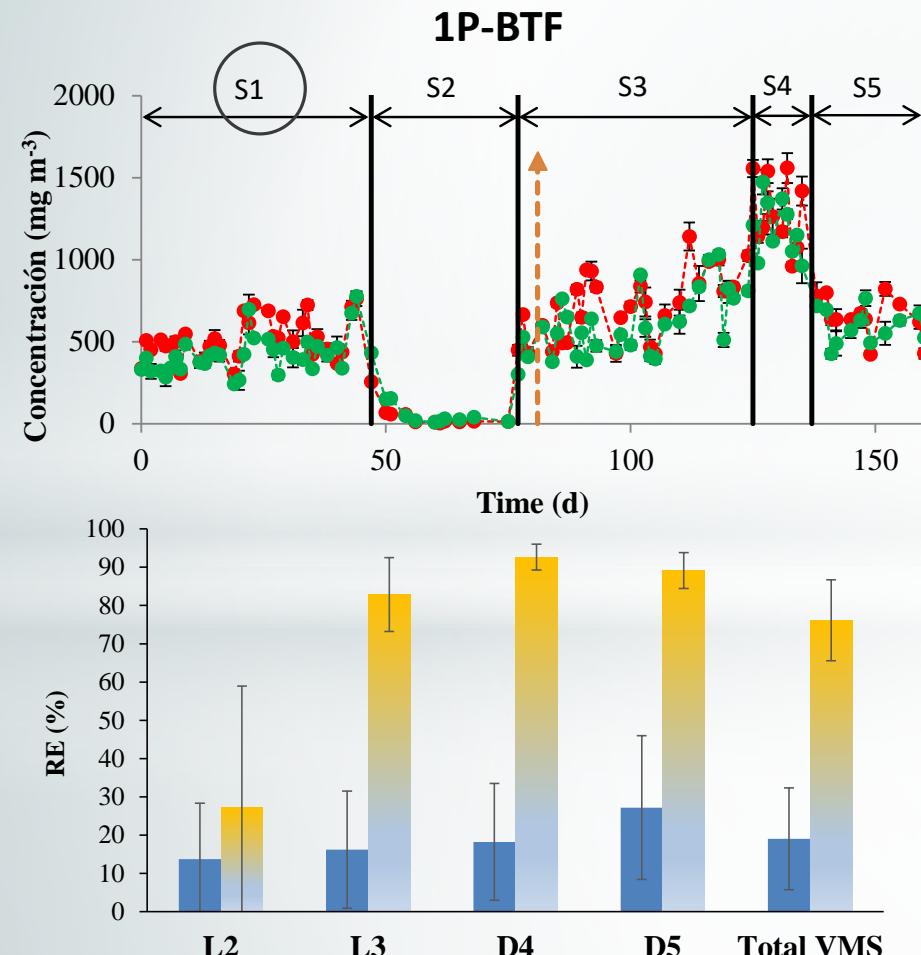


RE (%)



Inlet concentration (●)  
Outlet concentration (●)

# Total VMS removal - Comparative results



# Conclusions

- REs and ECs significantly higher in TP-BTF compared to 1P-BTF (~ 80 % higher)
  - VMS low solubility in aqueous phase
  - Reduced mass transfer
- The presence of an organic phase (silicon oil) is of key importance in VMS removal
- The highest REs were obtained for D4 and D5 (the compounds with highest molecular weight and lowest volatility)
- Future work:
  - Study of the microbial communities in siloxane removal TP-BTF
  - Metabolites analysis
  - Optimization of lab-scale BTF for siloxanes removal
    - Lower EBRT
    - VMS removal under anoxic conditions

# Thanks for your attention

## Biological removal of siloxanes from biogas for biomethane injection in natural gas grid

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